

# Energetic characterization of zeolites using a sensor gas calorimeter

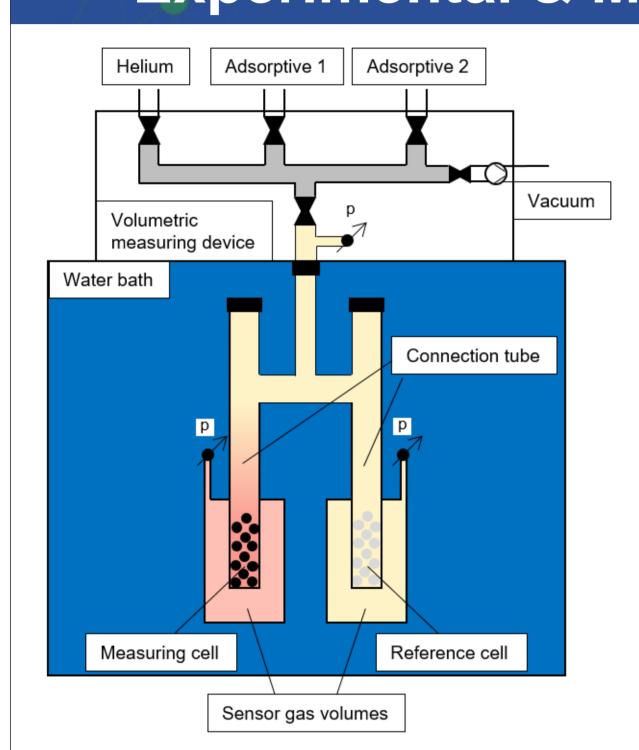
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# **Motivation & Targets**

Zeolites are often considered as homogeneous adsorbents. However, at a molecular level the zeolite structure consists of the framework and additional cations. The cations arrange themselves on different cation sites, which have different distances to the zeolite framework. Therefore, they are energetically heterogeneous. Until now, it is largely unknown which binding sites in zeolites are preferentially occupied by adsorptive molecules, which type of interactions are formed and what the energetic contributions of the respective binding partners are. Therefore, in this project we compare adsorption isotherms and heats of adsorption with XRD analyses on systematically modified zeolites. We aim to identify the different binding sites, to clarify the predominant interactions and to gain an understanding of the adsorption mechanisms taking place.

# **Experimental & Methods**



### Isotherm:

- Volumetric adsorption measurement (autosorb iQ 3)
- Cumulative measuring principle

### Load-dependent heat of adsorption:

- Combination of volumetric and calorimetric measurement
- Measurement of a time-dependent pressure difference between both sensor gas volumes
- Determination of heat of adsorption for each individual adsorption step

# Linde Type A (LTA) zeolites:

- Sodalite cages linked via D4R
- Zeolite framework consists of Si-, Al- and O-atoms
- Al-tetrahedra introduce negative charge
- Charge balancing through additional cations
- Cations are exchangeable (e.g. Na<sup>+</sup> was exchanged for Ca<sup>2+</sup>) Figure 2: Structure of LTA zeolite

the surface of the 4-rings All cation sites are accessible

Table 2: Calculated cation distribution in CaNaA zeolites

Na2

2.5

Ca1

Na1

**Cation sites** 

Ca2

0.5

Na3

Ca3

■ Na<sub>12</sub>A

Ca<sub>0.5</sub>Na<sub>11.0</sub>A

3 preferred cation positions

surface of the 6-rings

α-cage

Site I: In the α-cage on the

Site II: In the 8-ring of the

Site III: In the α-cage on

**Total number** 

12

11.5

11

6.5

Table 1: Thermodynamic and structural properties of methane

	Structure	Critical diameter	Dipole moment	Polarizability	Interactions
Methane		0.4 nm	0 D	2.59 · 10 <sup>-30</sup> m <sup>3</sup>	Induction Dispersion

**Zeolite** 

Na<sub>12</sub>A

Ca<sub>0.5</sub>Na<sub>11.0</sub>A

Ca<sub>1.1</sub>Na<sub>9.9</sub>A

Ca<sub>2.1</sub>Na<sub>7.7</sub>A

Ca<sub>2.8</sub>Na<sub>6.5</sub>A

Ca<sub>4.1</sub>Na<sub>3.8</sub>A

 $Ca_{5.4}Na_{1.2}A$ 

0.0

Figure 1: Schematic view of experimental setup

# Results & Discussion

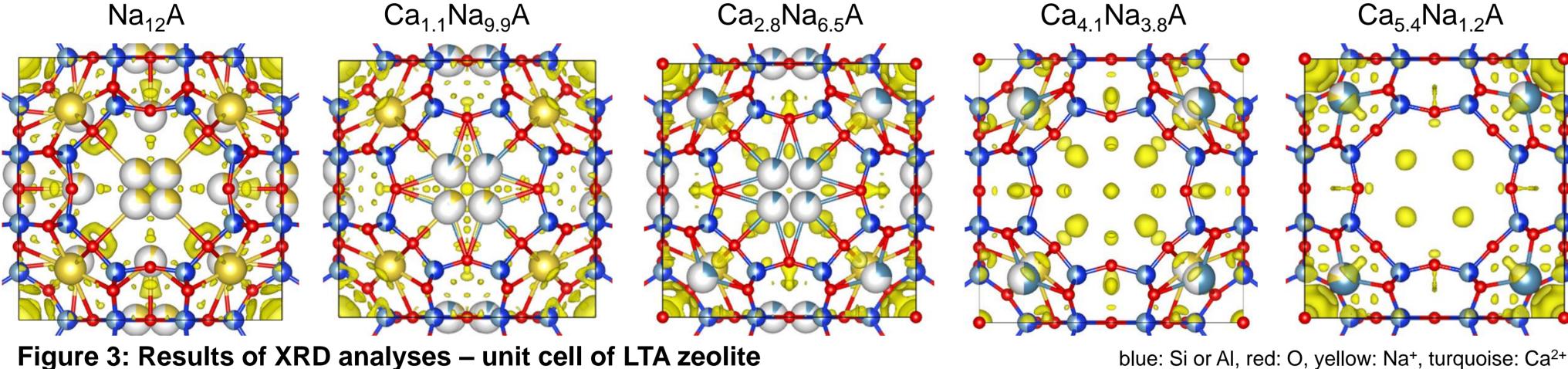


Figure 3: Results of XRD analyses – unit cell of LTA zeolite

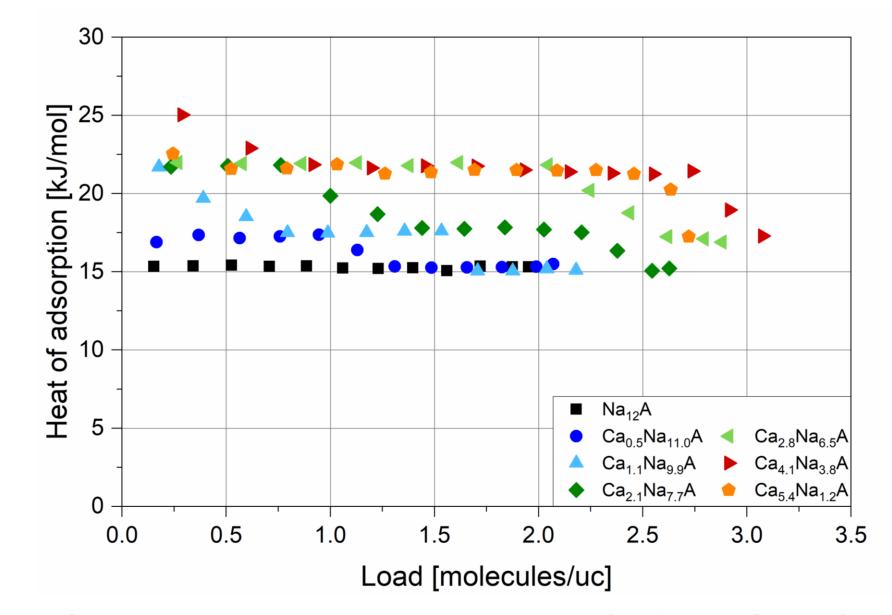


Figure 5: Load-dependent heats of adsorption of methane on CaNaA zeolites at 25 °C

- NaA: Constant heat of adsorption (HoA)
- CaNaA: Increasing HoA with increasing Ca<sup>2+</sup> content
- Calcium represent energetically higher adsorption sites
- Figure 6: Load-dependent heats of adsorption of methane on selected CaNaA zeolites at 25 °C

Load [molecules/uc]

- Plateau 15 kJ/mol: Na+ cations on site I
- Plateau 17.5 kJ/mol: Ca<sup>2+</sup> cations on site II
- Plateau 22.5 kJ/mol: Ca<sup>2+</sup> cations on site I

## Table 3: Energetic contributions of adsorption sites

	•		
Energetic contribution	kJ/mol		
Zeolite framework	≈ 12.5	•	
Na <sup>+</sup> on site I	<b>≈</b> 2.5		
Ca <sup>2+</sup> on site I	≈ 10.0		
Ca <sup>2+</sup> on site II	<b>≈</b> 5.0		

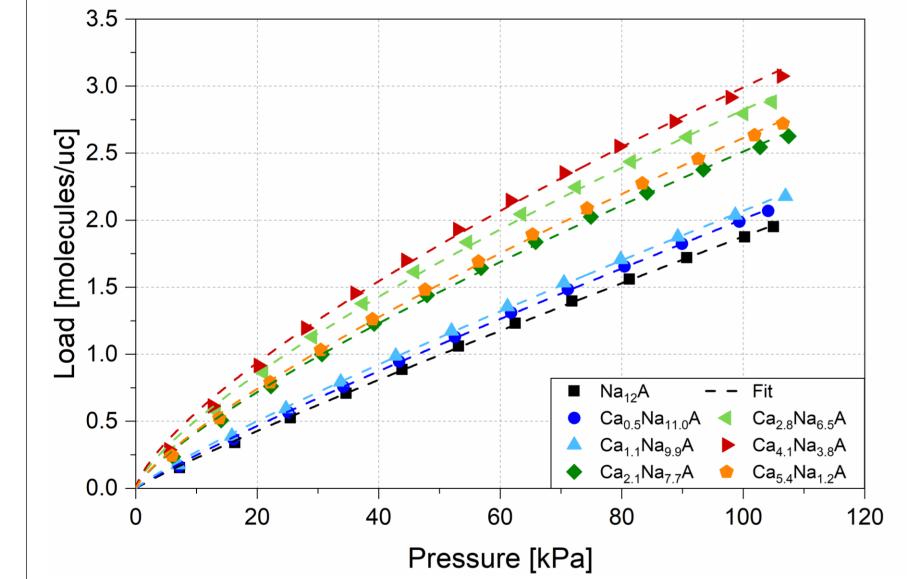


Figure 4: Adsorption isotherms of methane on CaNaA zeolites at 25 °C

- Freundlich isotherm at CaNaA zeolites
- Higher loading and curvature with higher Ca<sup>2+</sup> content
- Maximium in loading at a exchange rate of 69%

## Estimation of energetic contributions

Thermal induction interaction energy

$$\Phi_{Ind} = -\frac{q^2 \cdot \alpha}{2 \cdot 4\pi \varepsilon_0 \cdot r^4}$$

 $q = charge, \alpha = polarizability$ r = distance of interaction partners

- Assumptions
  - Ca<sup>2+</sup> has twice the charge of Na<sup>+</sup>
  - Polarizability remains constant
  - Ionic radii of Ca<sup>2+</sup> and Na<sup>+</sup> are similar
- System of equations
- (1)  $\Phi_{Ca^{2+}} = 4 \cdot \Phi_{Na^{+}}$ (2)  $\Phi_{Na^+,I} + \Phi_{FW} = 15 \text{ kJ/mol}$
- (3)  $\Phi_{Ca^{2+}J} + \Phi_{FW} = 22.5 \text{ kJ/mol}$
- (4)  $\Phi_{Ca^{2+},II} + \Phi_{FW} = 17.5 \text{ kJ/mol}$

# **Summary & Outlook**

For the energetic characterization of zeolites, adsorption isotherms and heats of adsorption were measured simultaneously. Additionally, XRD analyses were performed. The results on differently modified zeolites show significant differences in the loadings and heats of adsorption depending on the type and number of cations. For example, three different heat plateaus can be determined for the adsorption of methane on zeolite

Ca<sub>2.8</sub>Na<sub>6.5</sub>A. These indicate interactions with different cation sites. The XRD analyses show that Ca<sup>2+</sup> cations occupy cation site II ahead of site I. A combination of XRD results and heats of adsorption allows an estimation of the energetic contributions. It was found that the zeolite framework provides the largest energetic contribution. In future work, the influence of divalent cations, e.g. Mg<sup>2+</sup> or Ba<sup>2+</sup>, on adsorption will be further investigated.

# Acknowledgements

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